



Reaction Kinetics and Mechanistic Shift in Non/Catalytic Esterification of PEGs: Microwave-Assisted vs. Conventional Esterification

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Abstract

Esterification reactions play a crucial role in both industrial and biological systems, essential for the production of pharmaceuticals, polymers, and specialty chemicals. The esterification of polyethylene glycol (PEG) with chloroacetic acid (CAA) is important for surfactants, drug delivery systems, etc. This study investigates the esterification kinetics in a microwave-assisted, non-catalytic system, employing an alternative kinetic parameter estimation approach compared to conventional methods. Instead of separately analyzing temperature-dependent reaction rates, an optimization algorithm was used to simultaneously evaluate data from different temperatures. This novel method enhances the accuracy and reliability of kinetic parameters, while the absence of a catalyst significantly influenced the reaction mechanism, emphasizing the role of high-dielectric constant molecules. The esterification kinetics between CAA and PEGs were studied under both conventional and microwave-assisted conditions. Optimized kinetic data revealed that increasing PEG chain length resulted in decreased reaction rates, which was attributed to increased viscosity and steric hindrance effects. In the microwave method, lower rate constants were associated with the shorter thermal exposure of the reaction. Additionally, the collision frequency factor decreased with an increase in microwave power, due to the lower dielectric constants of PEG-based compounds. A significant change in reaction order was also observed under non-catalytic conditions; under microwave irradiation, PEG200 exhibited a reaction order of 1.5, while PEG400 showed second-order dependence. These findings offer new insights into the kinetic behavior of non-catalytic reactions and highlight the influence of molecular properties on reaction pathways. Ester formation was confirmed by FTIR and NMR analyses, providing evidence of successful esterification.

Keywords: Esterification, Microwave, Kinetic Study, Optimization, Reaction Mechanism Shift

1. Introduction

Esters are versatile compounds with a wide range of applications across various industries, owing to their unique properties and pleasant aromas [1]. They are found ubiquitously as both natural and synthetic organics [2]. In addition to their significant impact as fuels, plasticizers, solvents, flavoring, and aroma compounds, esters are also utilized in the synthesis of pharmaceutical and agricultural chemical compounds, in the cosmetic industry, and in personal care product formulations [2,3].

Esters are frequently employed in the synthesis of softeners, emulsifiers, dispersants, detergents, and surfactants [4]. Due to their numerous applications across various industries, research into the synthesis of more efficient esters has garnered considerable interest.

Esterification reactions generally proceed very slowly in the absence of a catalyst and are thermodynamically reversible [5]. Therefore, a catalyst is typically required to accelerate the reaction [6]. To shift the equilibrium towards the forward direction, either a homogeneous or heterogeneous acid catalyst should be used, and the water produced during the reaction must also be removed [7]. Commonly used homogeneous acid catalysts in esterification reactions include sulfuric acid (H₂SO₄), hydroiodic acid (HI), hydrofluoric acid (HF), phosphoric acid (H₃PO₄), para-toluenesulfonic acid (p-TSA), formic acid (HCOOH) [8], and aluminum chloride (AlCl₃), while heterogeneous acid catalysts include ion exchange resins, zeolites, triorganic acids, sulfate oxides, aqueous zirconium oxide, and supported heteropoly acids [9]. Recently, the use of enzymes as catalysts in

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esterification reactions has also gained attention [10,11].

The most common method for ester synthesis is catalytic, employing traditional heating techniques. However, traditional heating methods have some drawbacks, including long reaction times, uneven heating, high energy consumption, and low yields [12,13]. As an alternative to these methods, microwave-assisted heating, a novel energy source, is widely used [14]. Since microwave radiation can directly interact with materials at the molecular level, it provides uniform and rapid heating of reactants [15]. This rapid heating occurs due to ionic conduction or dipole rotation, which increases molecular dynamics. More intense molecular movements lead to more energetic collisions, thus enhancing the reaction rate [12]. As a result, high yields and purity products are obtained in short reaction times [14]. In the literature, studies involving the use of fatty acids and amino alcohols [16,17,18], diols [19], halogenated alcohols [20], alkyl diamines [21], acid chlorides [22], polyethylene glycols [203], alcohols [13,24,25], acids [26], and glycerol [27] as reactants in esterification reactions can be found. Additionally, studies have explored the use of acyl halides with diamines [28], polyols [29], and diols [30,31]. Furthermore, Dabiri and Honarvar (2020) studied the esterification of sunflower oil and glycerol [32], Chauhan et al. (2023) investigated the esterification of epoxy esters with imidazole [33], Shaban et al. (2022) examined the esterification of two different carboxylic acids [34], Sripada and Kastner (2023), and Huang et al. (2024) researched the esterification of an acid and alcohol [35], [36], and Lin et al. (2025) studied the esterification of gluten and starch [37], while Wang et al. (2022) investigated the esterification reaction of carboxylic acids and alcohols [38]. Fashi et al. (2024) conducted a study in which they performed microwave-assisted solid-state acetic acid esterification of corn starch and examined its structural and functional effects [39]. Using Zn-Mg-Al catalysts, Abas et al. (2020) employed microwave-assisted heating to achieve maximum conversion in the esterification of lauric acid with diethylene glycol [40]. In another study, artificial neural networks were used to predict the yield of biodiesel produced from palm oil fatty acid distillate using a TiO₂-ZnO mesoporous catalyst under microwave heating [41]. Tarigan et al. (2025) used calcined waste egg shells as a catalyst to produce biodiesel from high-fatty acid feedstocks under microwave irradiation [42]. Umrigar et al. (2022) synthesized biodiesel, known as mono alkyl esters of fatty acids, using oleic acid and various alcohols (methanol, ethanol, 2-propanol) under

microwave-assisted conditions [43]. Sitepu et al. (2023) reported the microwave-assisted enzymatic esterification of various fatty acids (myristic and palmitic) with isopropyl alcohol, resulting in energy savings [44]. In their study, Akream et al. (2024) synthesized biodiesel from waste cooking oils under microwave-assisted conditions with a bi-functional ZnO-Ce/AC catalyst, achieving 99.6% yield [45]. Nayak et al. (2021) performed microwave-assisted esterification of kusum oil with silicotungstic acid, achieving 99.6% yield and found that microwave energy reduced the activation energy [46]. Lieu et al. (2016) applied a microwave-assisted esterification pre-treatment to reduce the free fatty acid content of seed oil with high free fatty acid content, achieving esterification with 94.43% yield [47]. Johari et al. (2024) studied the kinetic aspects of microwave-assisted transesterification of dairy waste scum oil in the presence of a catalyst, and compared it with a study using the same feedstock with traditional methods [48].

The chemical structure and chain length of reactants in a chemical reaction significantly influence both the molecular properties and the kinetics of the synthesis process. Although the literature includes several studies involving polyethylene glycol (PEG) derivatives with varying chain lengths, investigations focusing on short-chain PEGs remain limited. Furthermore, the effect of PEG chain length on the kinetics of esterification reactions has not been adequately clarified. In addition, a comprehensive comparative analysis of the kinetic behavior under conventional and microwave-assisted methods is lacking.

This study aims to determine the kinetic parameters of esterification reactions between PEGs of different molecular weights (PEG 200 and PEG 400) and chloroacetic acid under both conventional and microwave-assisted conditions (Figure 1). Before proceeding with the temperature-dependent experiments, preliminary trials performed under conventional conditions without a catalyst revealed that the reaction progressed rather slowly. Therefore, p-toluenesulfonic acid (p-TSA) was employed as a homogeneous catalyst in the conventional method. In the microwave-assisted method, however, the catalyst was not used, as it was observed to degrade under microwave irradiation. In both methods, the progress of the reaction was monitored using a titrimetric method, with methanol as the solvent, phenolphthalein as the indicator, and 0.5 N potassium hydroxide as the titrant. The experimental data obtained were analyzed using an optimization algorithm, and the kinetic

parameters of the reactions were determined and compared. In this context, the hypothesis that an increase in PEG chain length reduces the reaction rate and that the microwave-assisted method exhibits a distinct kinetic profile was tested.

2. Experimental Section

2.1. Chemical Reagents and Properties

Polyethylene glycol (200) (CAS No: 25322-68-3, Ataman Chem.), polyethylene glycol (400) (CAS No: 25322-68-3, Sözal Chem. Inc.), chloroacetic acid (CAS No: 79-11-8, $\geq 99\%$, Merck), methanol (CAS No: 67-56-1, $\geq 99.7\%$, Honeywell), potassium hydroxide (CAS No: 1310-58-3, $\geq 86\%$, Sigma-Aldrich), phenolphthalein (CAS No: 77-09-8, Merck), petroleum ether (CAS No: 64742-49-0, $\geq 86\%$, Kimyalab), and diethyl ether (CAS No: 60-29-7, $\geq 99.7\%$, Sigma-Aldrich) are the chemicals used in the experiments. All chemicals were used directly without any additional purification process.

Microwave reactions were carried out using a Milestone Ethos Easy microwave system (MA174-001) in a round-bottom flask with constant stirring speed (30%) and variable temperature using microwave power (max 450W).

The FTIR analysis of the synthesized polyethylene glycol chloro-esters (PEG_nClEs) in this study was performed using a Perkin Elmer Spectrum Two model device located in the Chemistry Department at Bursa Technical University.

The ¹HNMR analysis of the synthesized polyethylene glycol chloro-esters (PEG_nClEs) in this study was performed using a JEOL ECZ500R (11.75 Tesla) spectrometer located at the Central Research Laboratory (ARUM) of Eskişehir Osmangazi University.

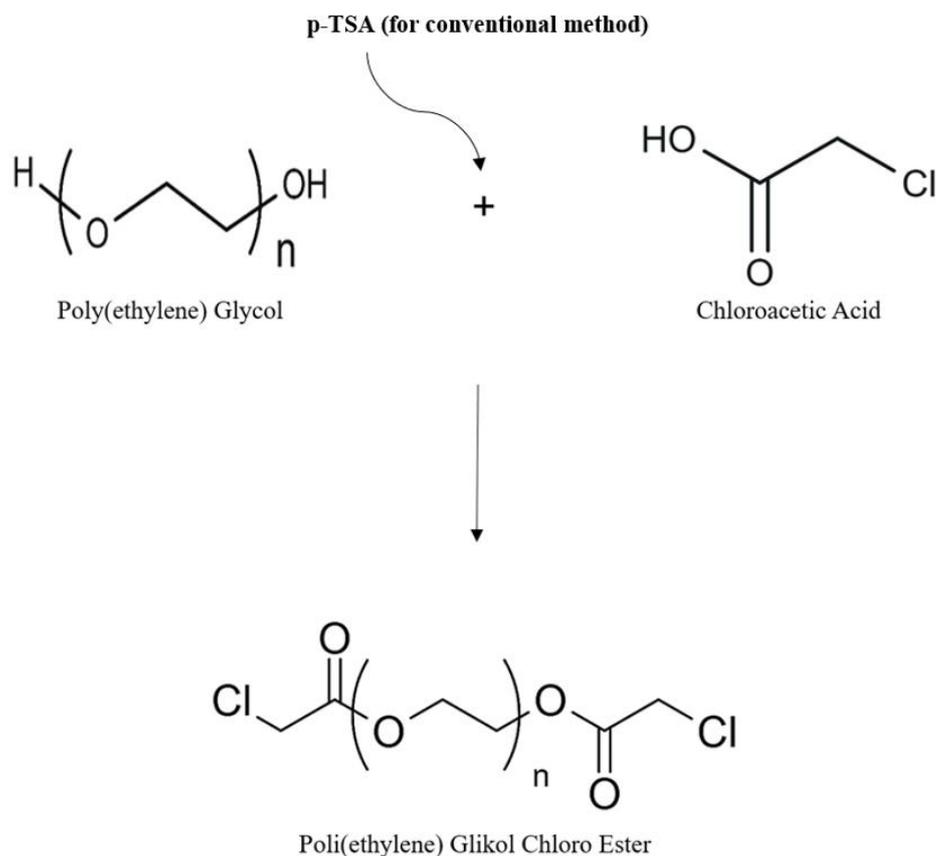


Figure 1. Molecular representation of the synthesis process for poly(ethylene glycol) chloroesters.

2.2. Experimental Procedure

In the conventional method, PEG_nClEs were prepared through the esterification of 0.2 mol chloroacetic acid

with 0.1 mol polyethylene glycol (PEG200 and PEG400) separately. As a catalyst, 0.01% p-Toluen Sulfonic Acid (p-TSA) was added to the reaction. The

reactions were carried out at various temperatures under atmospheric pressure, and the water formed during the reaction was removed using a Dean-Stark apparatus (Figure 2a). The catalyst was removed from the final reaction mixture using petroleum ether [49,50]. In the microwave method, PEG_nClEs was prepared through the microwave irradiation of 0.2 mol

chloroacetic acid with 0.1 mol polyethylene glycol (PEG200 and PEG400) separately. No catalyst was used in the microwave experiments. The reactions were performed at various temperatures under atmospheric pressure, and the water formed during the reaction was removed using the same procedure as in the conventional method (Figure 2b) [51].

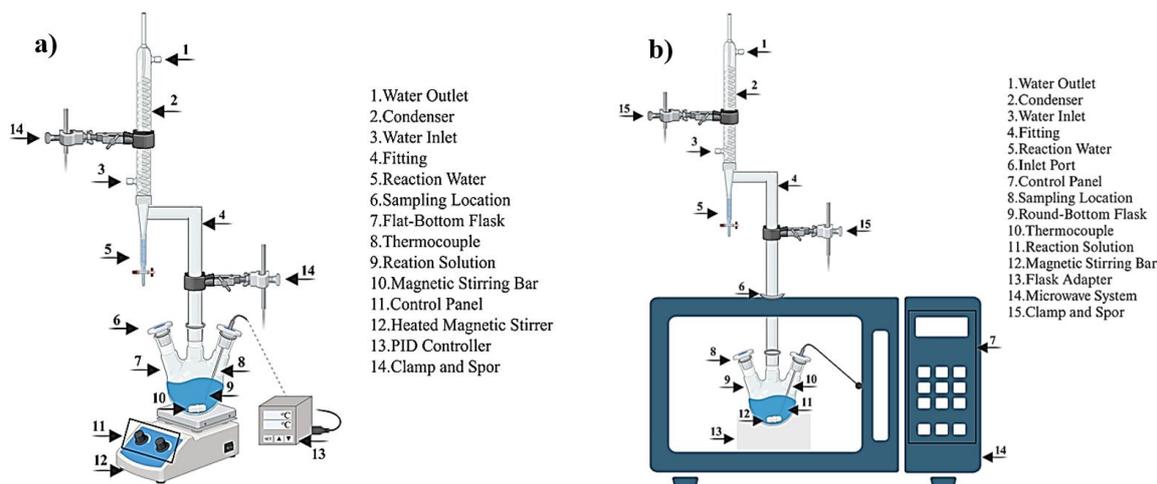


Figure 2. Schematic diagram of experiment setup a) conventional method b) microwave method.

2.3. Kinetic Study

The polyethylene glycol esterification reaction with chloroacetic acid carried out in this study is a bidirectional reaction. In this case, the esterification reaction occurs as a result of 1 mol of polyethylene glycol reacting with 2 mol of chloroacetic acid. The reactants consumed and the products formed in the reaction are encoded as shown in Eq. (1).



Here, A represents polyethylene glycol, B represents chloroacetic acid, C represents polyethylene glycol chloroester, and D represents the water formed as a result of the reaction. The water formed during the reaction was collected and removed, ensuring that the reaction proceeded in one direction. Therefore, the rate equation for the esterification reaction of polyethylene glycol with chloroacetic acid can be expressed as shown in Eq. (2).

$$-r_A = k \cdot [C_A]^a \cdot [C_B]^b \quad (2)$$

Here, C_A represents the concentration of polyethylene glycol and C_B represents the concentration of

chloroacetic acid at time t . k is the rate constant of the reaction, and a and b represent the reaction orders. In this reaction occurring in the liquid phase, the average densities are taken into account, and the following mole balance equation for liquid-phase reactions is obtained. To determine the stoichiometric coefficients in this equation, Eq. (2) and (3) provided below were used to derive Eq. (4) and (5).

$$\frac{dC_A}{dt} = r_A \quad (3)$$

$$-C_{A0} \cdot \frac{dX}{dt} = r_A = -k \cdot [C_A]^a \cdot [C_B]^b \quad (4)$$

$$\begin{aligned} \frac{dX}{dt} &= \frac{-r_A}{C_{A0}} \\ &= \frac{k \cdot [C_{A0}(1-X)]^a \cdot [C_{B0}(1-2X)]^b}{C_{A0}} \end{aligned} \quad (5)$$

Here, X represents the conversion of polyethylene glycol at time t , and C_{A0} and C_{B0} represent the initial concentrations of polyethylene glycol and chloroacetic acid, respectively. To determine the reaction rate constant parameters, samples were taken from the reaction at different time intervals, and titration was performed using a solution KOH

prepared with methanol at a specific concentration. For titration, 0.5 g of the product was dissolved in 20 mL of methanol, and phenolphthalein indicator was added, followed by titration with KOH solution. The amount of KOH consumed (mL) was recorded, and the conversion at time t was calculated.

Additionally, for various reaction temperatures, the reaction orders (a and b) and the reaction rate constants (k) were determined according to the kinetic model that best fit the data from both the conventional and microwave methods. Subsequently, a regression was performed using the ideal gas constant (R) and reaction temperatures (T), and the activation energies (E_a) and Arrhenius constants (A) were calculated based on the Arrhenius equation given in Eq. (6).

$$k = A \cdot e^{\frac{-E_a}{RT}} \quad (6)$$

The steps taken to determine the kinetic parameters are outlined in the flowchart in Figure (3). In this study, a comparison of the reaction kinetic parameters obtained for both methods, was conducted.

3. Results and Discussion

3.1. Optimization of Kinetic Model Parameters

In the microwave studies conducted with PEG200, reactions were carried out at temperatures of 110 °C, 138 °C, and 150 °C, and conversion values were obtained. In the conventional method, these studies were conducted at 90 °C, 110 °C, and 138 °C in the presence of a catalyst. The graph of conversions obtained by optimizing kinetic parameters using experimental data and model equations, along with the correlation coefficients, is shown in Figure (4).

In the microwave method with PEG400, studies were conducted at temperatures of 110 °C, 138 °C, and 150 °C, while in the conventional method, studies were carried out at 110 °C, 125 °C, and 138 °C with the presence of a catalyst, and conversions were obtained. The graph of conversions obtained by optimizing the kinetic parameters using experimental data and model equations, along with the correlation coefficients, is shown in Figure (5).

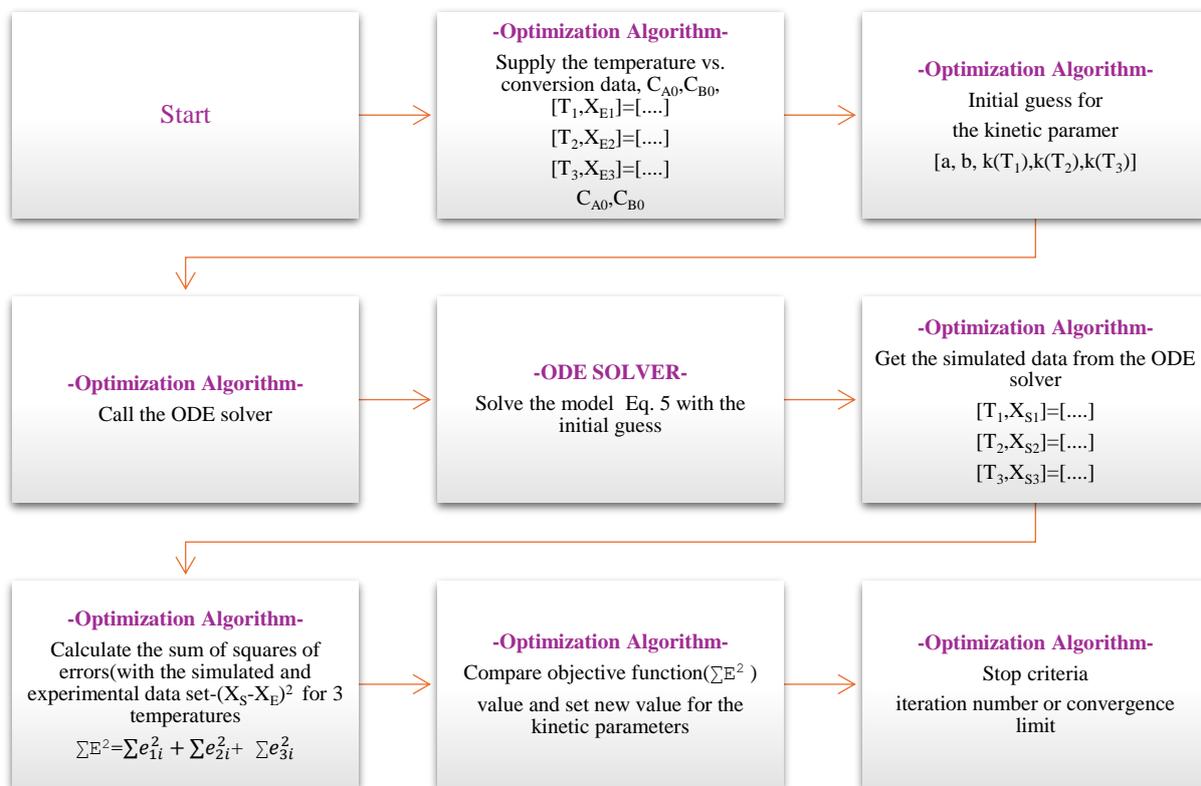


Figure 3. Kinetic parameter Optimization procedure flow diagram.

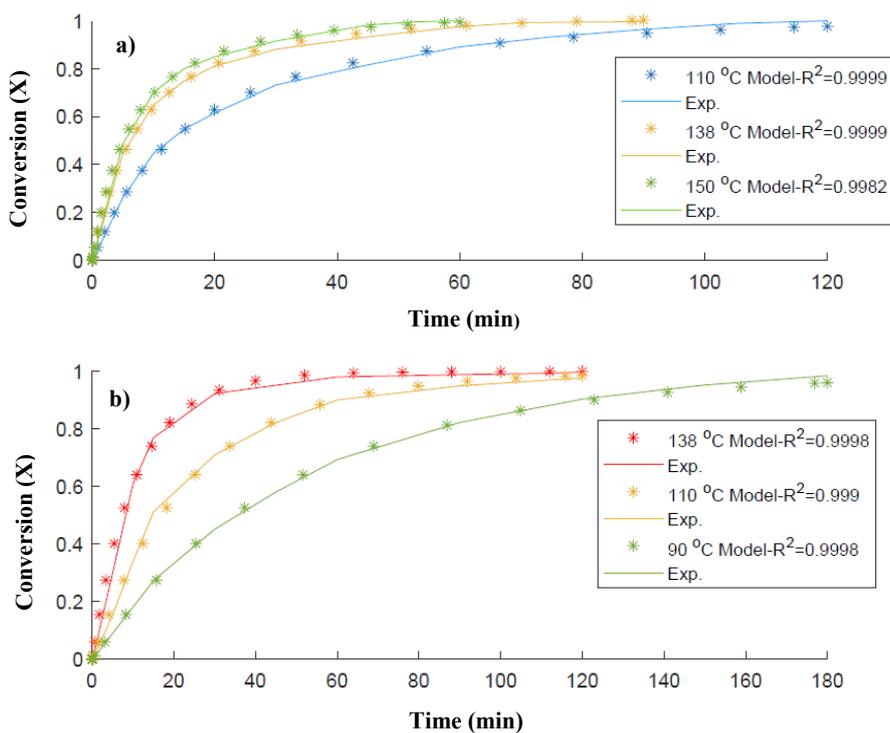


Figure 4. Experimental and simulation results of conversion (X) curves for reactions carried out at different temperatures using PEG200: a) microwave method, b) conventional method.

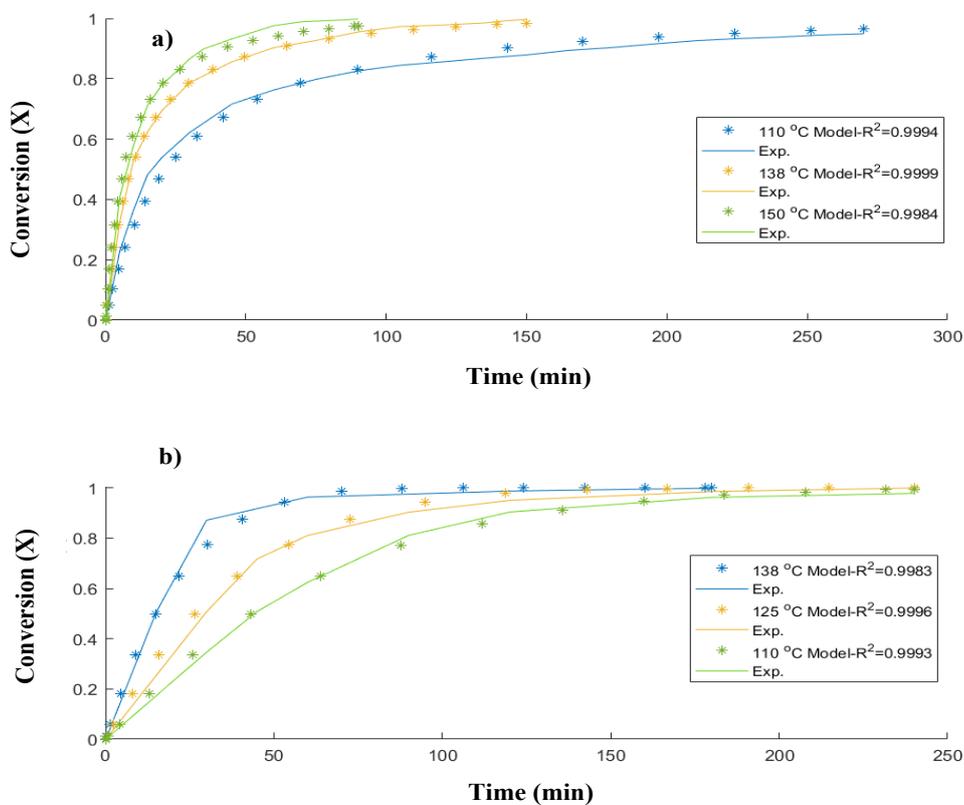


Figure 5. Experimental and simulation results of conversion (X) curves for reactions carried out at different temperatures using PEG400: a) microwave method, b) conventional method.

In both methods (Traditional and Microwave), high correlation coefficients and maximum fit were observed for PEG200 and PEG400, indicating that the model fits the experimental data very well. The increase in temperature led to a rapid increase in conversions, showing an exponential effect. This can be explained by the increase in molecular kinetic energy as the temperature rises, which results in a higher number of successful collisions and, consequently, an increase in reaction rate and conversion. The shorter reaction times for PEG200 are attributed to its lower molecular weight, shorter chain length, and viscosity, which allows for higher reactivity. As a result, the reactions with PEG200 were completed faster. In the catalytic experiments, PEG200 reached a conversion of 95% in 120 minutes, while for PEG400, this time extended to 180 minutes. When a catalyst was used, the conversion times for both PEG200 and PEG400 significantly decreased; a

conversion of 92% and 87% was achieved in 30 minutes, respectively. It was also observed that the effect of the microwave method was nearly identical to the catalyst effect, and microwave experiments produced similar conversion times to the catalyst-assisted traditional methods. Notably, for PEG200, conversions above 98% were observed in 50 minutes at 138 °C, while for PEG400, these conversions were achieved in both methods in approximately 70 minutes. These findings suggest that both microwave and catalyst-assisted methods showed very similar effects, but the processes for PEG200 were completed faster.

Additionally, in order to more clearly observe the effect of the catalyst in the conventional method, experiments were conducted at the same temperature without the catalyst. The obtained results are presented in Figure 6.

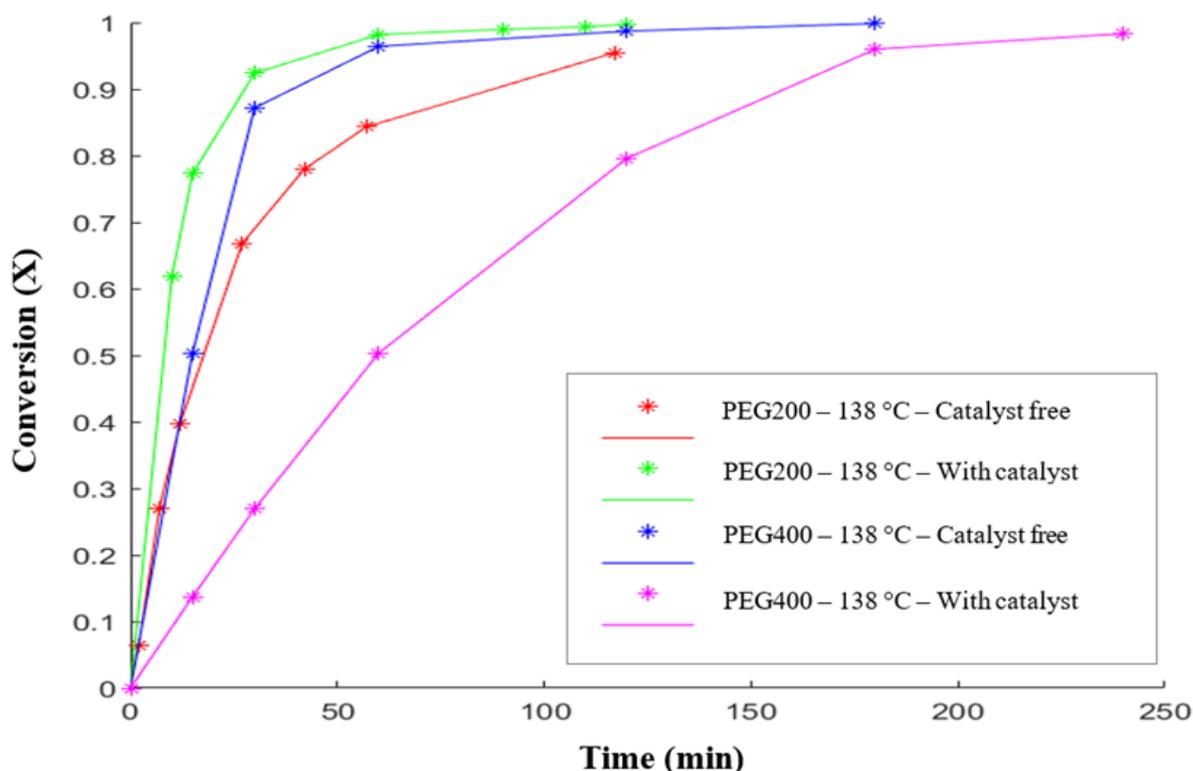


Figure 6. Catalyst effect on conversion (X) of reactions performed with PEG200 and PEG400 at 138°C using the conventional method.

The figure demonstrates a significant increase in reaction rate in the presence of the catalyst. In the absence of the catalyst, longer reaction times were required to reach the same level of conversion. This

result indicates that the catalyst enhances the reaction kinetics by lowering the activation energy and thereby accelerates the reaction process.

In the microwave system, catalyst-assisted experiments were also conducted. However, the p-Toluenesulfonic acid (p-TSA) catalyst was found to be affected and degraded by microwave energy, so no catalyst was used in the microwave experiments. In the traditional method, it was observed that catalyst-free experiments were quite slow, but catalyst-free

microwave experiments produced almost identical results to the catalyst-assisted traditional method experiments. By utilizing kinetic study data and the Arrhenius equation, the rate constants for the esterification reactions were calculated, and the values are provided in Table 1.

Table 1. Calculated reaction rate constants determined at different reaction temperatures.

Conventional		Microwave	
<i>PEG₂₀₀CIEs (with catalyst)</i>		<i>PEG₂₀₀CIEs (catalyst free)</i>	
<u>T(K)</u>	<u>K</u>	<u>T(K)</u>	<u>k</u>
411	0.0885	423	0.0249
383	0.0383	411	0.0202
363	0.0187	383	0.0098
<i>PEG₄₀₀CIEs (with catalyst)</i>		<i>PEG₄₀₀CIEs (catalyst free)</i>	
<u>T(K)</u>	<u>K</u>	<u>T(K)</u>	<u>k</u>
411	0.0492	423	0.0158
398	0.0275	411	0.0110
383	0.0169	383	0.0047

When examining the effect of temperature on the reaction rate constant, it was observed that the rate constant increased with rising temperature for each experiment. The fundamental reason for this increase is the collisions that occur due to the enhanced

mobility of molecules at higher temperatures [54,55]. Based on the kinetic study data and the Arrhenius equation, the stoichiometric coefficients, Arrhenius constants, and activation energies for the conducted esterification reactions are provided in Table 2.

Table 2. Detailed kinetic data obtained from the reaction under various conditions, supported by optimization studies.

Conventional		Microwave	
<i>PEG₂₀₀CIEs (with catalyst)</i>		<i>PEG₂₀₀CIEs (catalyst free)</i>	
a	1.0775	A	0.1339
b	0.0054	B	1.5261
A	11279.02	A	221.0967
Ea/R	4830.6	Ea/R	3837.2
<i>PEG₄₀₀CIEs (with catalyst)</i>		<i>PEG₄₀₀CIEs (catalyst free)</i>	
a	0.8675	a	0.0046
b	0.0025	b	1.9949
A	95894.13	A	1626.686
Ea/R	5970.5	Ea/R	4888.4

When the data presented in Tables 1 and 2 are analyzed, it is evident that the conventional and MW methods provide significantly different results. In the conventional method, the reaction appears to follow approximately first-order kinetics for PEG200 and PEG400, while for CAA, it seems to follow zero-order kinetics (considering experimental errors and initial assumptions). In the MW method, where no catalyst is used, it is believed that the reaction mechanism changes completely. When PEG200 is used as a

reactant, the reaction follows first-order kinetics with respect to CAA, and when PEG400 is used, the reaction follows second-order kinetics with respect to CAA.

In the MW method, the key parameter is thought to be the dielectric constant of CAA (ϵ_{CAA} : 33.4). This is because PEGs have a much lower dielectric constant (ϵ_{PEG200} : 12.5, ϵ_{PEG400} : 17.5), and the chain length of the PEG is considered to be the major factor in the

reaction mechanism. In the microwave method, the Arrhenius constant is approximately 50-60 times smaller than in the conventional method. This decrease can be related to the microwave absorption and collision theory. The activation energy for the reactions also decreases by about 25%, strengthening the reaction's dependence on concentration, which allows the reactions to be completed much faster compared to the conventional method.

As a result, in the conventional method with a catalyst, PEG200 achieves 98% conversion in 60 minutes, and PEG400 achieves 96% conversion, while without a catalyst, the conversions are 84% and 50%,

respectively, over the same time. The MW method, on its own, can nearly match the catalytic effect, achieving similar conversion rates. These results are consistent with other findings reported in the literature [56-59].

3.2. Characterization of the Esterification Product by FTIR and $^1\text{H-NMR}$

In order to support the structural verification of the synthesized products, Fourier Transform Infrared (FTIR) spectroscopy analyses were conducted, and the resulting spectra are presented in Figure 7. This analysis was performed to assess whether the esterification reaction proceeded successfully.

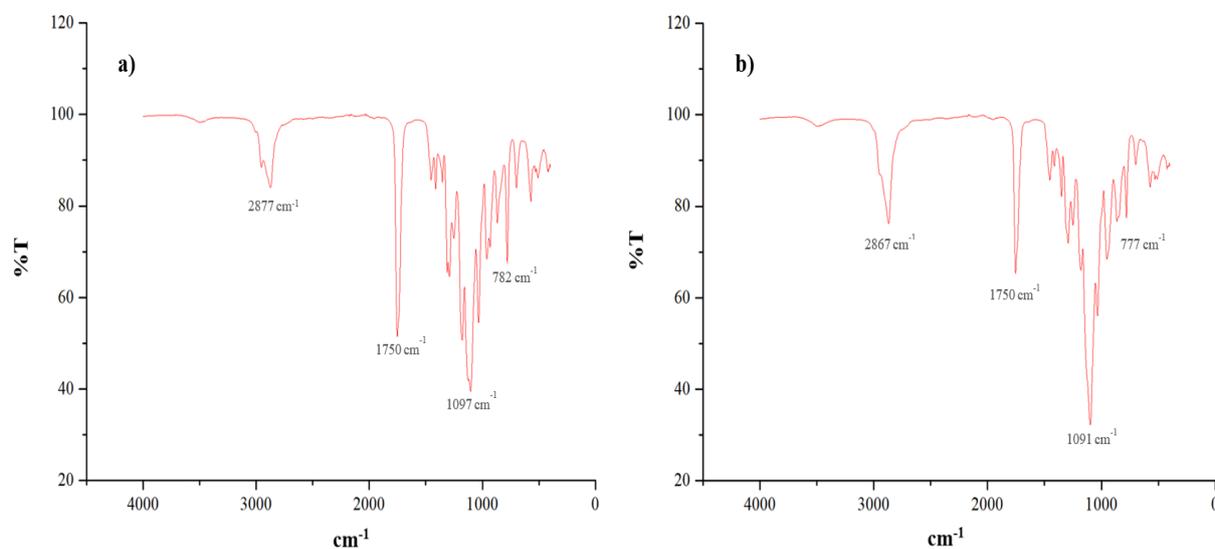


Figure 7. FT-IR spectra of synthesized polyethylene glycol chloro-esters a) PEG₂₀₀CIEs b) PEG₄₀₀CIEs

The FTIR spectra of the reactants are provided in the supplementary information. Figure S1 is the FTIR spectrum of chloroacetic acid. The peaks observed in the range of 3200–3570 cm^{-1} in Figure S2 and S3 are attributed to OH stretching vibrations [60–62]. Upon examining both spectra, it is observed that the broad peaks at 3442 cm^{-1} and 3411 cm^{-1} almost completely disappear in the PEG₂₀₀CIEs and PEG₄₀₀CIEs spectra. This indicates that water is absent in the final products. The peaks in the range of 2845–2977 cm^{-1} represent $-\text{CH}_2$ stretching vibrations [63,64]. The presence of peaks at the same positions in both the PEG spectra and the spectra of the synthesized products indicates that PEG molecules are still present in the final product.

The peaks in the 1700–1725 cm^{-1} range are attributed to the C=O stretching of carboxylic acids, while the peaks in the 1725–1750 cm^{-1} range are attributed to ester group C=O stretching vibrations [60]. The peak at 1750 cm^{-1} in the PEG₄₀₀CIEs and PEG₂₀₀CIEs

spectra indicates the formation of the ester bond. The peaks in the 1050–1150 cm^{-1} range represent the stretching vibrations of C-O-C bonds [64]. The peaks at 1091 cm^{-1} in PEG₄₀₀CIEs and 1097 cm^{-1} in PEG₂₀₀CIEs show the presence of PEG molecules in the final product. The peaks in the 600–800 cm^{-1} range are attributed to C-Cl stretching vibrations [60,65]. The peaks at 777 cm^{-1} in PEG₄₀₀CIEs and 782 cm^{-1} in PEG₂₀₀CIEs indicate the presence of chlorine from chloroacetic acid in the final product. Overall, the FT-IR spectra provide strong evidence that the synthesis of the intended (PEG_nCIEs) was successfully achieved.

The $^1\text{H-NMR}$ spectra recorded in DMSO- d_6 confirmed the chemical structure of the synthesized polyethylene glycol chloroesters (PEG₂₀₀CIEs and PEG₄₀₀CIEs). The polyethylene glycol chloroesters have the same proton distribution. Only the number of repeating ethylene oxide units in each structure

differs. The spectrum obtained for PEG₂₀₀CIEs is presented in Figure 8.

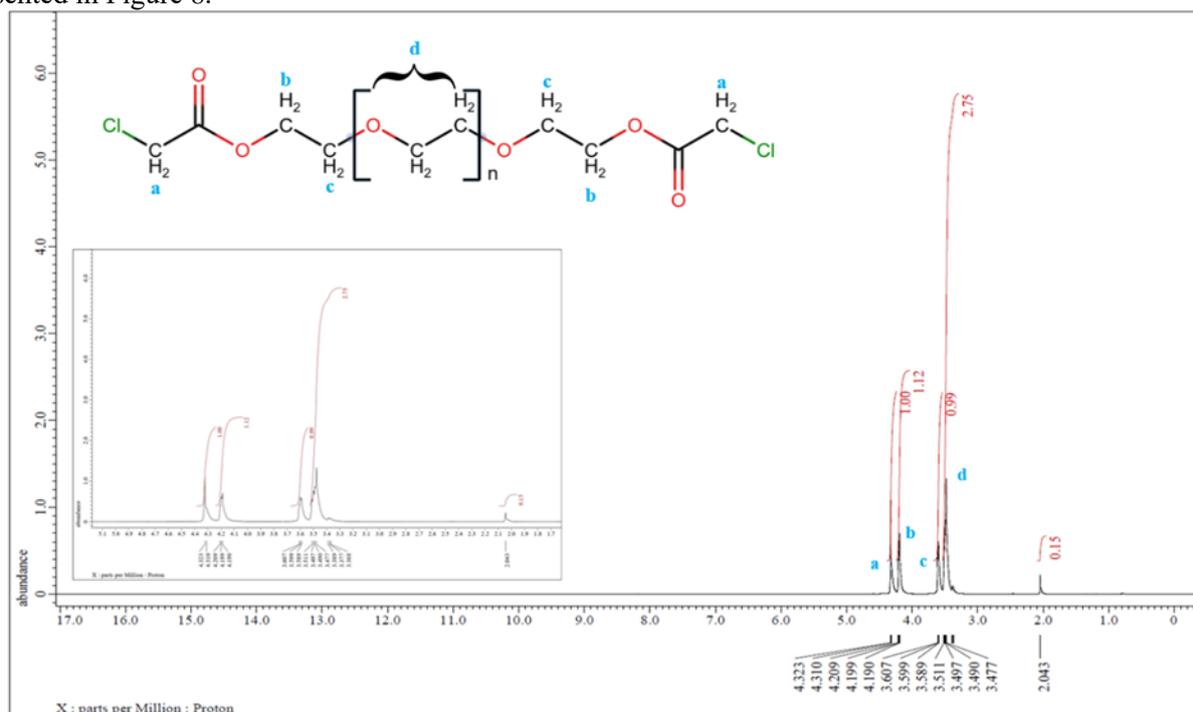


Figure 8. ¹H-NMR Spectrum of the synthesized PEG₂₀₀CIEs.

As a result of the characterization studies of the product, the information obtained from the FT-IR spectrum was confirmed by the NMR spectrum. Based on the results, it was concluded that the polyethylene chloro(di)ester structure was successfully synthesized as intended.

4. Conclusions

The results of this study underscore the advantages of employing an optimization-based approach for kinetic parameter estimation, particularly when dealing with multi-temperature datasets. The simultaneous analysis of reaction kinetics across different temperatures allowed for a more comprehensive and reliable parameter determination compared to conventional stepwise methods. Additionally, the absence of a catalyst led to a mechanistic shift in the reaction, where high-dielectric constant molecules played a more pronounced role. The esterification of PEG with chloroacetic acid represents an important reaction pathway for synthesizing functionalized polymeric materials with tailored physicochemical properties. By understanding the kinetic parameters governing this reaction, it is possible to optimize reaction conditions for enhanced product yield and efficiency. The ability to manipulate reaction orders through microwave-assisted methods further broadens the scope of esterification applications, particularly in solvent-free or low-energy synthesis approaches. The reaction order analysis further confirmed that the non-

catalytic microwave-assisted process follows a distinctly different kinetic regime. In conventional catalyzed reactions, PEG followed a first-order reaction, whereas microwave-assisted non-catalytic conditions caused the reaction order to shift to 1.5 and 2 for PEG₂₀₀ and PEG₄₀₀, respectively. This suggests that the role of dielectric properties is more prominent in determining reaction kinetics, as the interaction of chloroacetic acid with PEG molecules is facilitated by its significantly higher dielectric constant. Moreover, the observed decline in collision frequency with increasing microwave power supports the hypothesis that PEG's lower dielectric constant reduces its interaction probability under these conditions. These findings contribute to a deeper understanding of reaction kinetics in non-catalytic environments and open new perspectives for future kinetic modeling and reaction engineering strategies.

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Declarations

Conflict of interest The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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